



LARGE SCALE TRANSPORT OF BIOMASS FEEDSTOCK THROUGH PIPELINE FOR PRODUCTION OF FUELS AND CHEMICALS

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IEA BIOENERGY – BIOFUELNET WORKSHOP

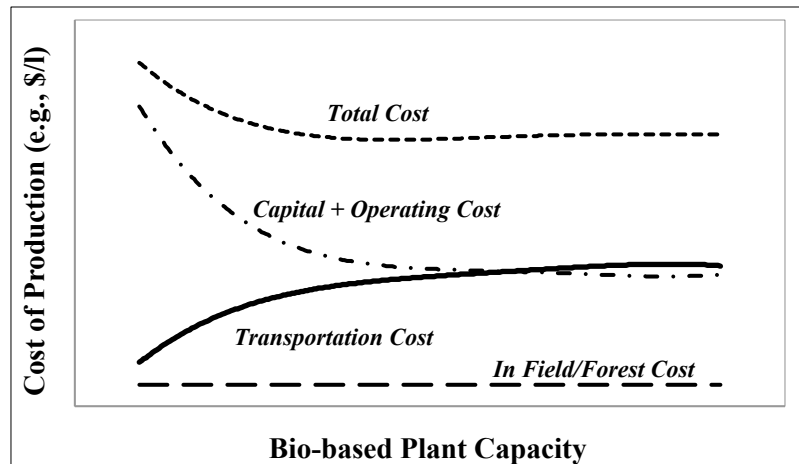
SEPTEMBER 22, 2016

UBC, VANCOUVER, CANADA



RESEARCH MOTIVATION

Optimum size of field/forest based biomass facility



Ruth, 1999
Jenkins, 1997



Corbis.com

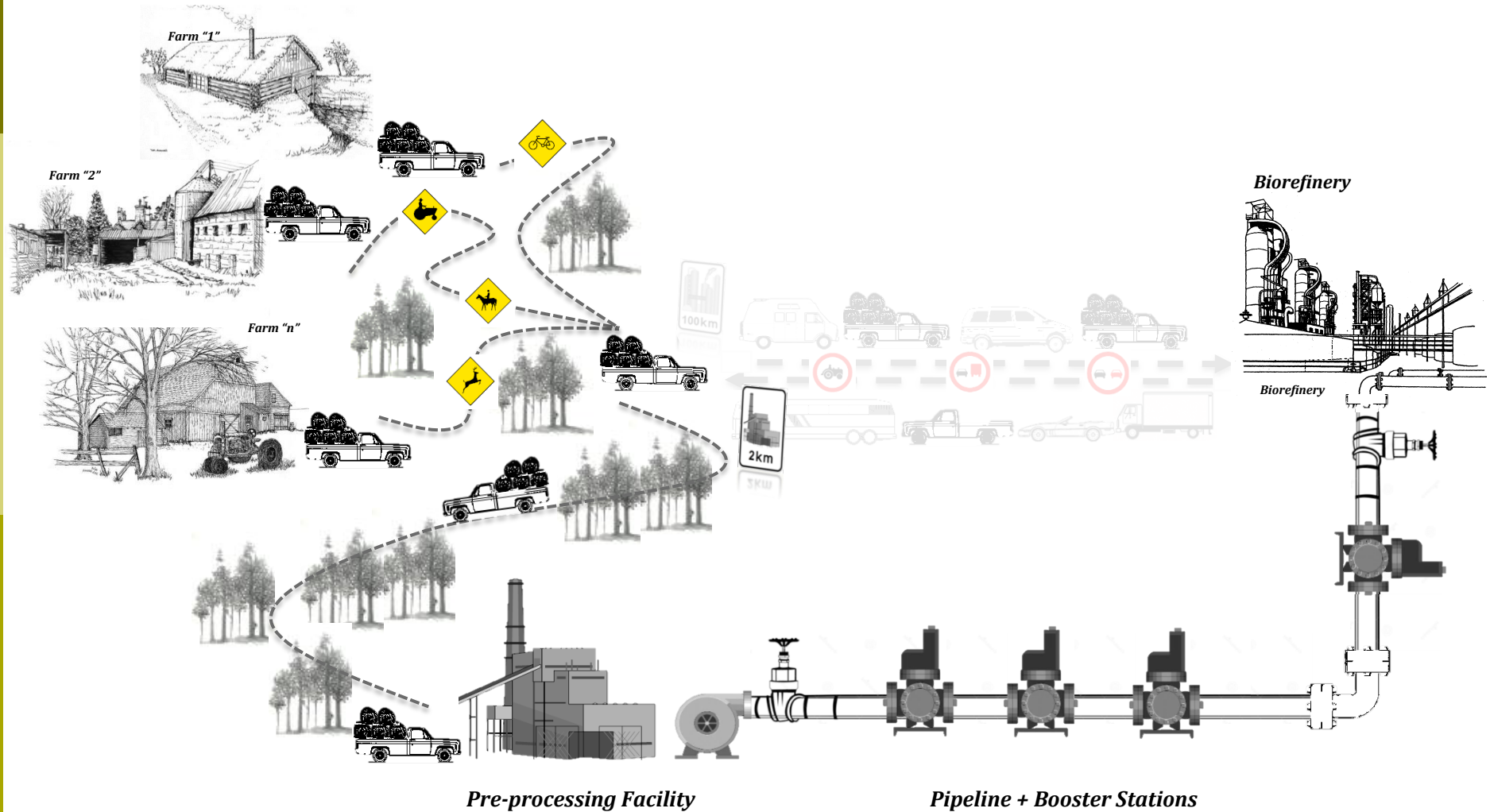
Issues in large-scale utilization of biomass

- ❑ 2 M dry t corn stover per year
- ❑ Logistics: 15 standard highway trucks per hour
- ❑ Producing 20,000 barrel (0.2 Ml) ethanol daily
- ❑ Typical oil refinery capacity over 850,000 barrel (10 Ml) daily
- ❑ 4.3 M t of wood chips per year
- ❑ Logistics: one chip van (36 t capacity) every four minutes
- ❑ Producing 900 MW electricity (typical fossil fuel-based power plant capacity)

Kumar et al., 2003 & 2004

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THE IDEA OF BIOMASS PIPELINE HYDRO-TRANSPORT



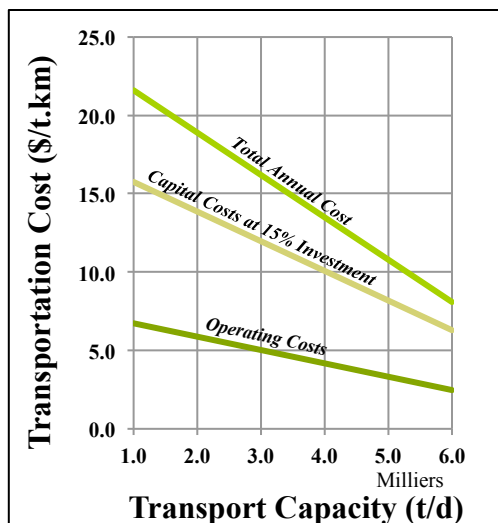


HISTORY OF BIOMASS PIPELINE HYDRO-TRANSPORT

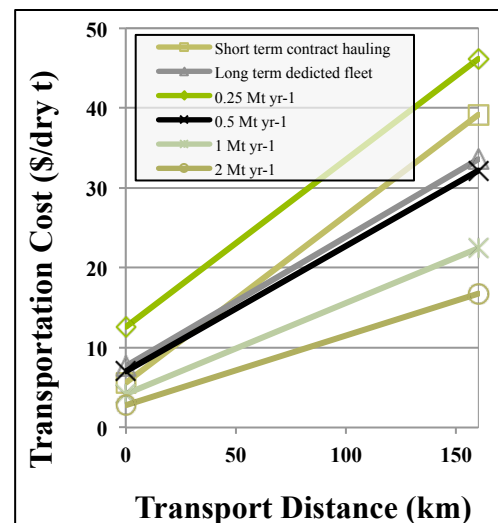
Technical feasibility of biomass pipeline hydro-transport

- ❑ Nora Blatch, Cornell University, 1906
- ❑ Pipeline transport of wood chip-water mixture (laboratory-scale), PAPRICAN, 1960's
- ❑ Pipeline transport of wood pulp suspensions (short distance), Pulp and paper industry
- ❑ No study on pipeline hydro-transport of agricultural residue biomass

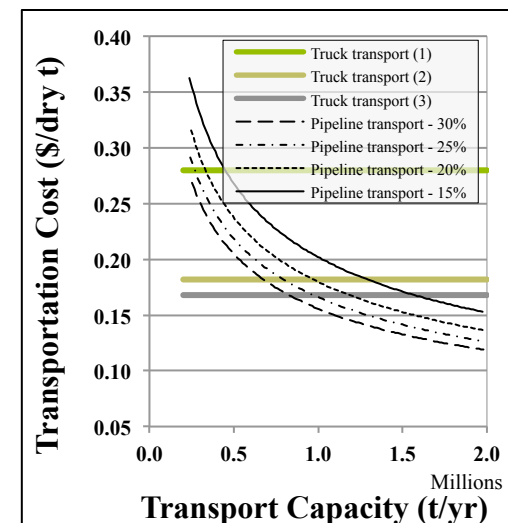
Economic feasibility of biomass pipeline hydro-transport



Wasp et al., 1967



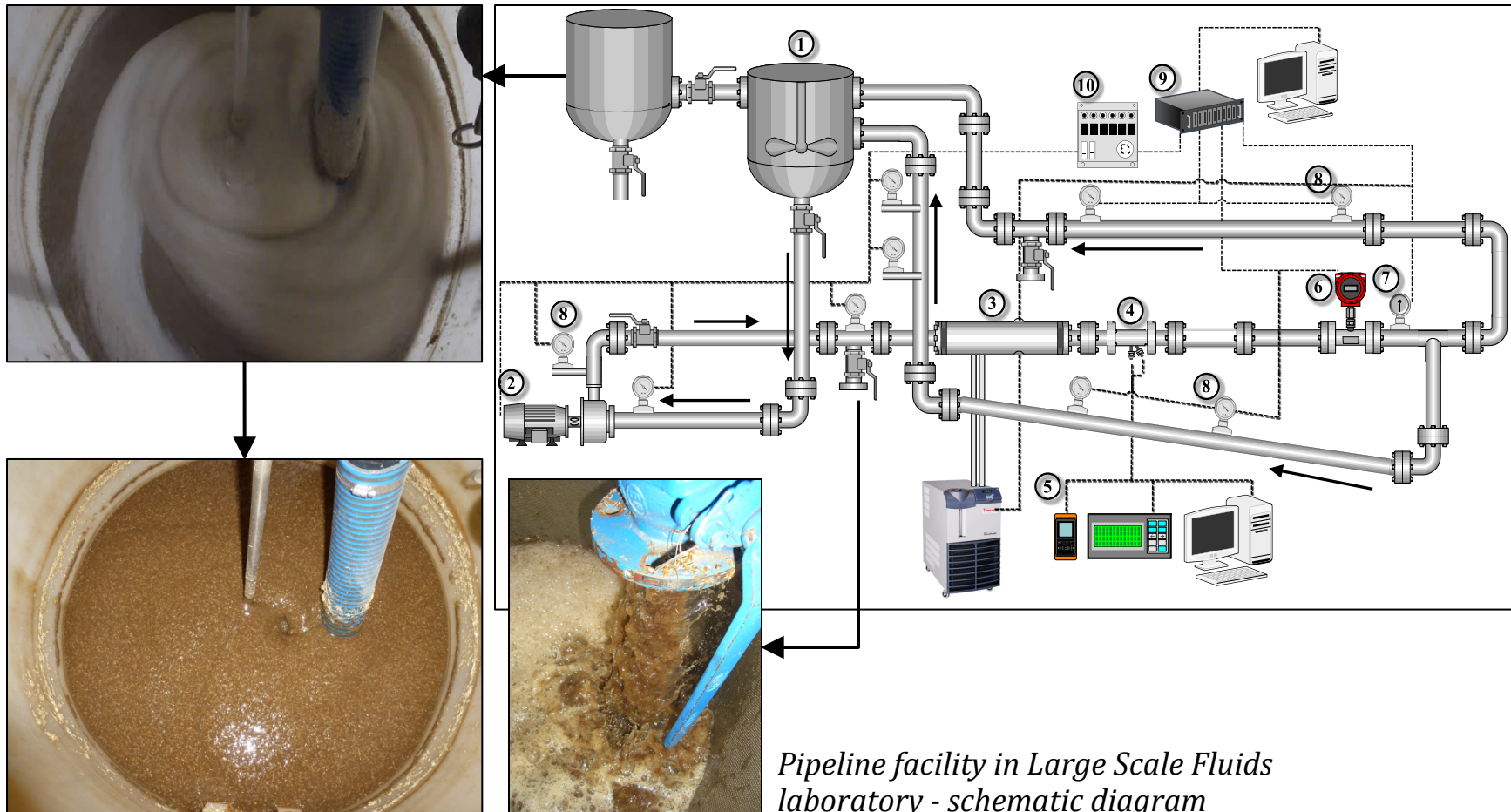
Kumar et al., 2004



Kumar et al., 2005



EXPERIMENTAL METHODOLOGY IN LARGE-SCALE FLUIDS LABORATORY AT UOFA



Pipeline facility in Large Scale Fluids laboratory - schematic diagram



PARTICLE SIZE ANALYSIS (CamSizer® P4)

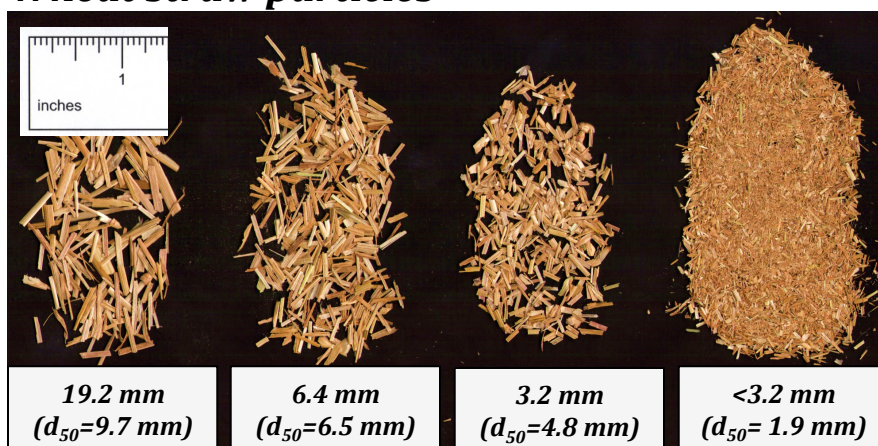
Woodchips particles



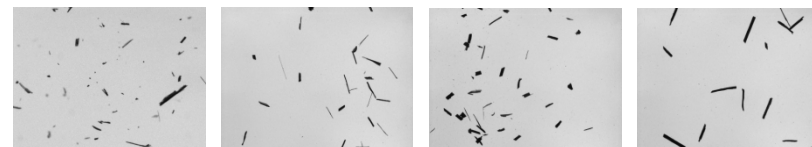
CamSizer Realtime Photos



Wheat straw particles



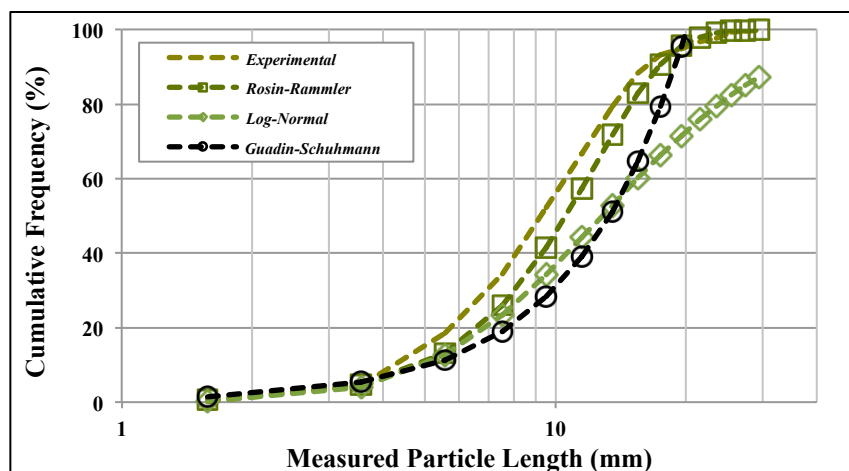
CamSizer Realtime Photos



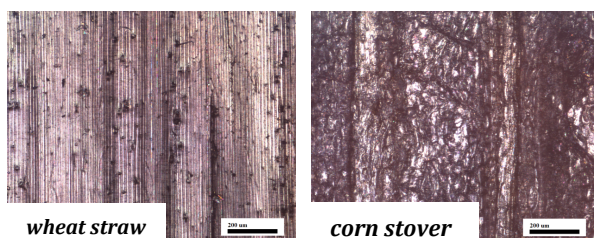
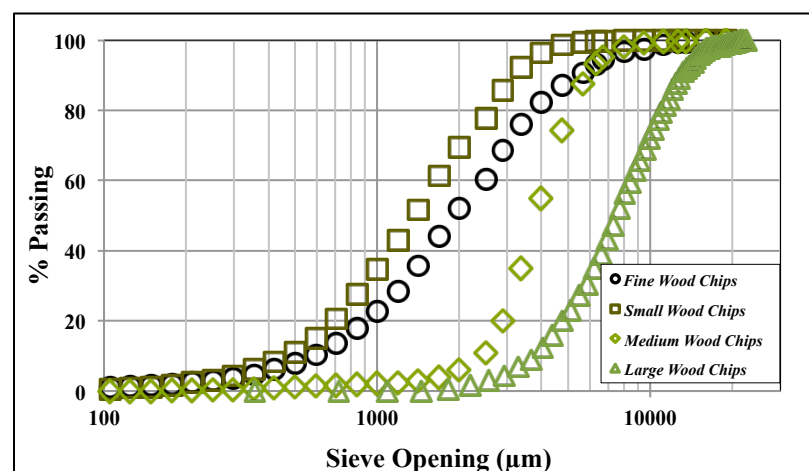


PARTICLE SIZE ANALYSIS (Digital Image Processing)

Triple distribution functions and image analysis of 19.2 mm (3/4") corn stover



Accumulative particle size distribution of woodchips particles



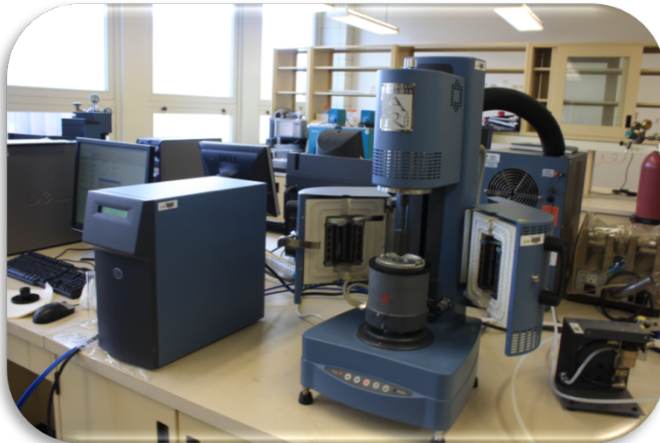
Confocal scanning microscope images of wheat straw and corn stover particles at 10x magnification

Material	Average Roughness (μm)	Highest Peak (μm)	Lowest Valley (μm)	Kurtois
Wheat Straw	7.9	130.2	149.9	9.3
Corn Stover	53.1	207.3	250.8	3.3

*J. Biosystems Engineering
Vaezi et. al., 2013*



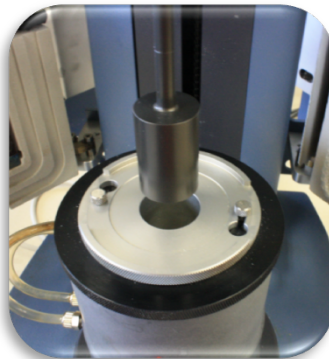
SLURRY RHEOLOGICAL MEASUREMENTS



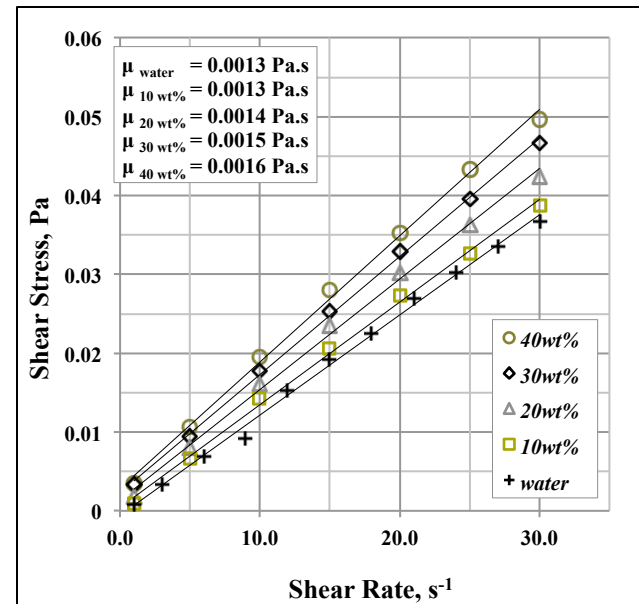
Rotational viscometer (AR 2000; TA Instrument, New Castle, DE, US) with concentric cylinder geometry



Slurry Filtration Process



Concentric Cylinder Geometry



Viscosity of the filtered carrier fluid of 10 to 40 wt% suspensions of <1/8" wheat straw particles at 15°C

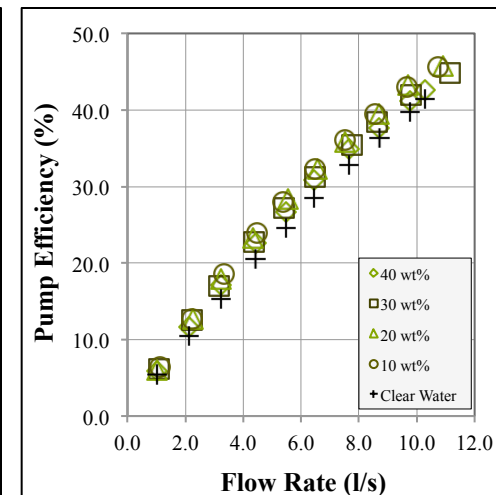
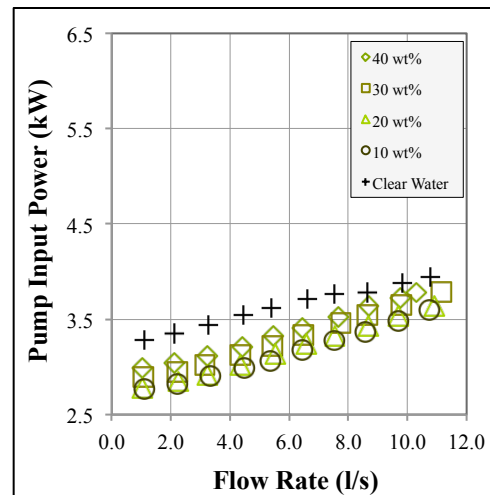
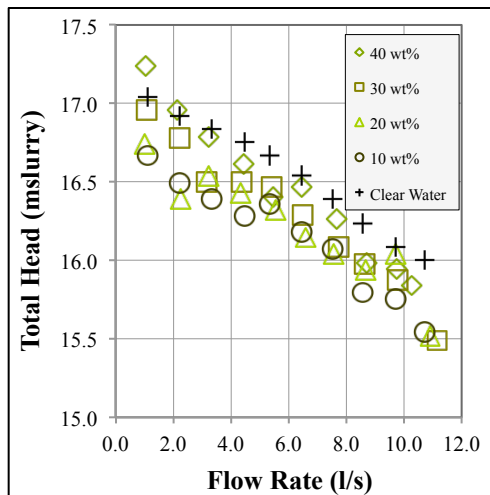
Vaezi et al, Investigation into the mechanisms of pipeline transport of slurries of wheat straw and corn stover to supply a bio-refinery, J. Biosystems Engineering, 2014



PUMP PERFORMANCE EVALUATION

Centrifugal slurry pump performance evaluation

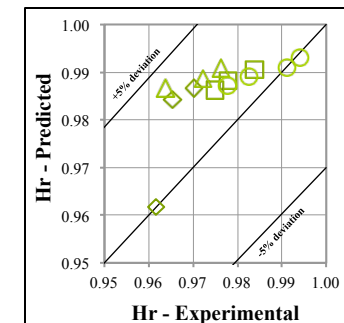
Performance characteristics of $<1/8"$ wheat straw particles slurries at 1765 rpm



Empirical correlation development

to predict the head ratio while pumping agricultural residue biomass slurry with less than 5% deviation

$$H_r = 1 - [(0.4C_w - 0.3)(0.1d_{50}^{1/2} + 28)]$$

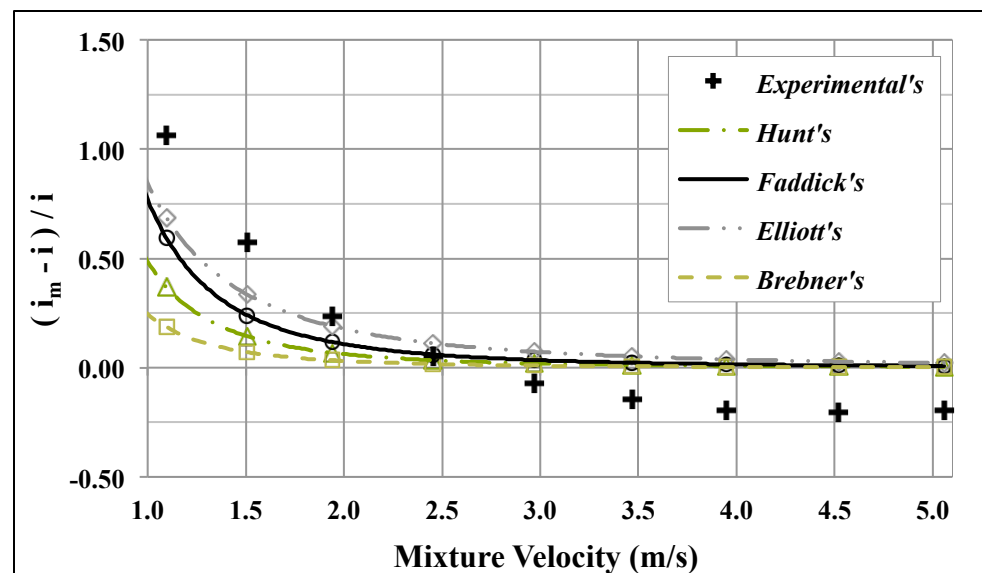




WOOD CHIPS CORRELATIONS APPLICABILITY

Friction loss behavior comparison

Empirical correlations by Hunt (1976), Faddick (1963), Elliot (1963), and Brebner (1964)



Friction loss parameter vs.
mixture velocity for 6.5% slurry of
6.4 mm corn stover particles

$$\text{Hunt's: } \left(\frac{i_m - i}{i} \right) = 197 \left(\frac{D_{pipe}^{0.97} g^{1.312} v^{0.342}}{V_m^{2.964}} \right) \left(\frac{C_v}{1 - C_v} \right)^{0.838 + 0.93 \ln(1 - k)}$$

$$\text{Elliot's: } \left(\frac{i_m - i}{i} \right) = 211 C_v \left(\frac{D_{pipe}^{0.5}}{V_m} \right)^{2.25}$$

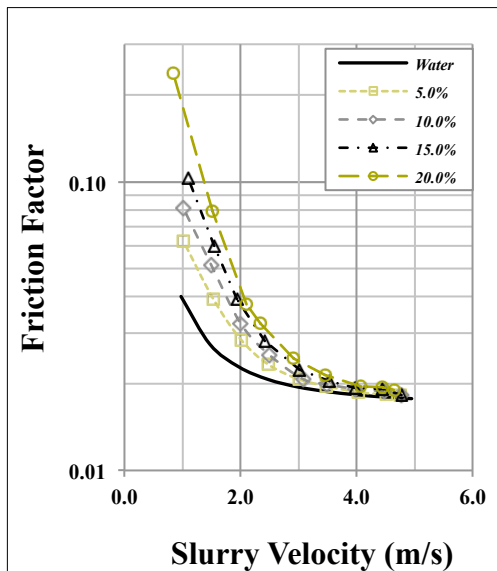
$$\text{Faddick's: } \left(\frac{i_m - i}{i} \right) = 2.51 C_v \left(\frac{4 g D_{pipe}}{V_m^2} \right)^{1.42}$$

$$\text{Brebner's: } \left(\frac{i_m - i}{i} \right) \cong 18 C_v \left(\frac{V_m^2}{g D_{pipe}} \right)^{-1.5}$$

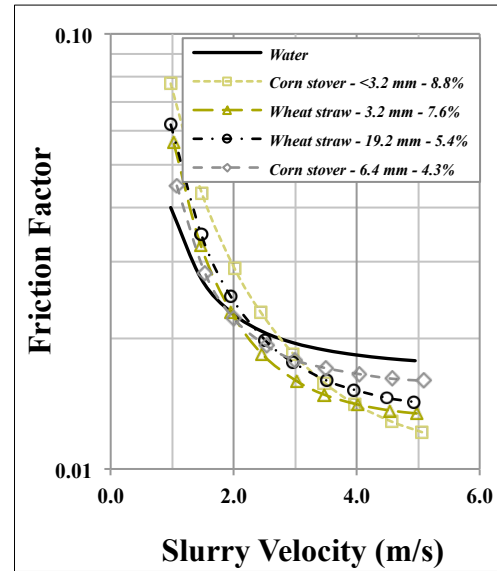


FRICTION LOSS BEHAVIOUR STUDY

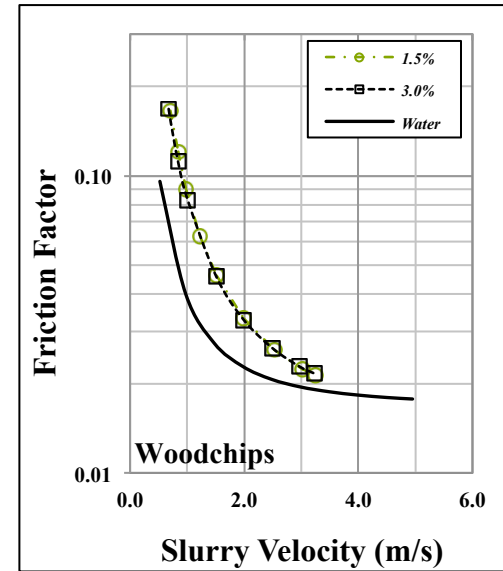
Sand, wheat straw and woodchips longitudinal friction loss measurements



play sand particles



*wheat straw particles
wood fibers*



Woodchips

Slurry friction loss correlation development

$$\Delta H/L = \left[\sum_{n=1}^3 \alpha_n S_n + \beta_n V_n + \gamma_n C_n + \delta_n V_n \right]$$

Coefficients for numerical correlation

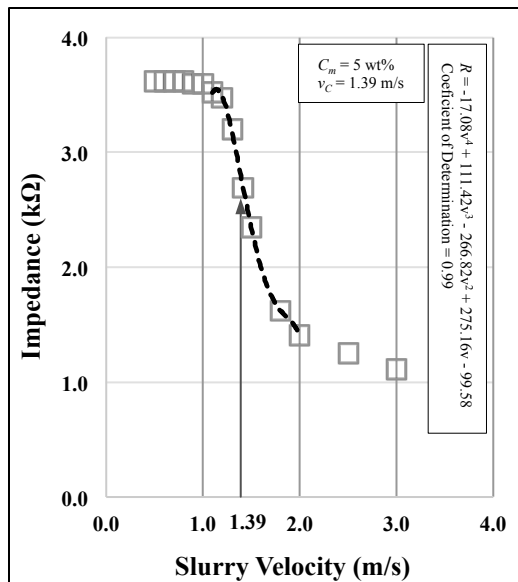
Coefficient	Dummy		
	$n = 1$	$n = 2$	$n = 3$
α	1.22465	-1.97098	0.64855
β	0.00000	0.16389	0.00000
γ	0.00000	0.00000	0.00066
δ	0.00000	-0.00104	0.00000
D_0	0.0508 m		

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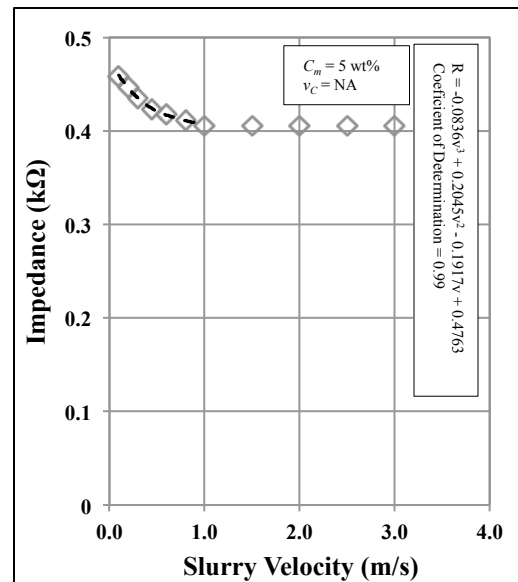


CRITICAL SETTLING VELOCITY CALCULATION

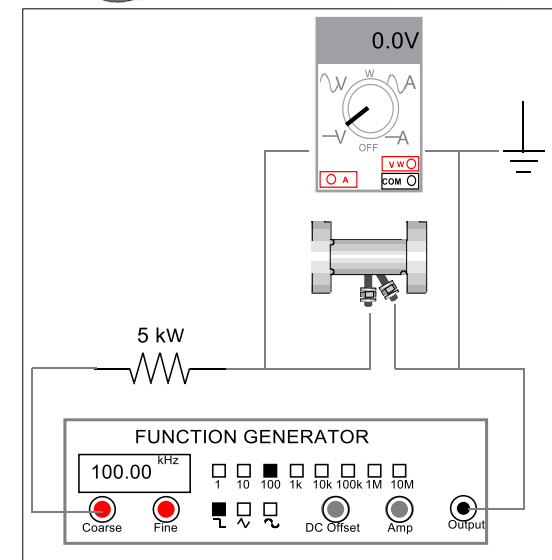
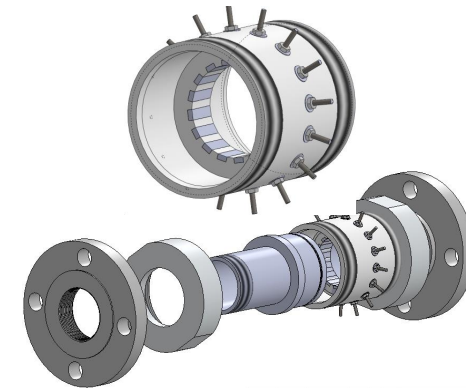
High-Frequency Impedancemetry to Calculate Critical Settling Velocity



Play Sand



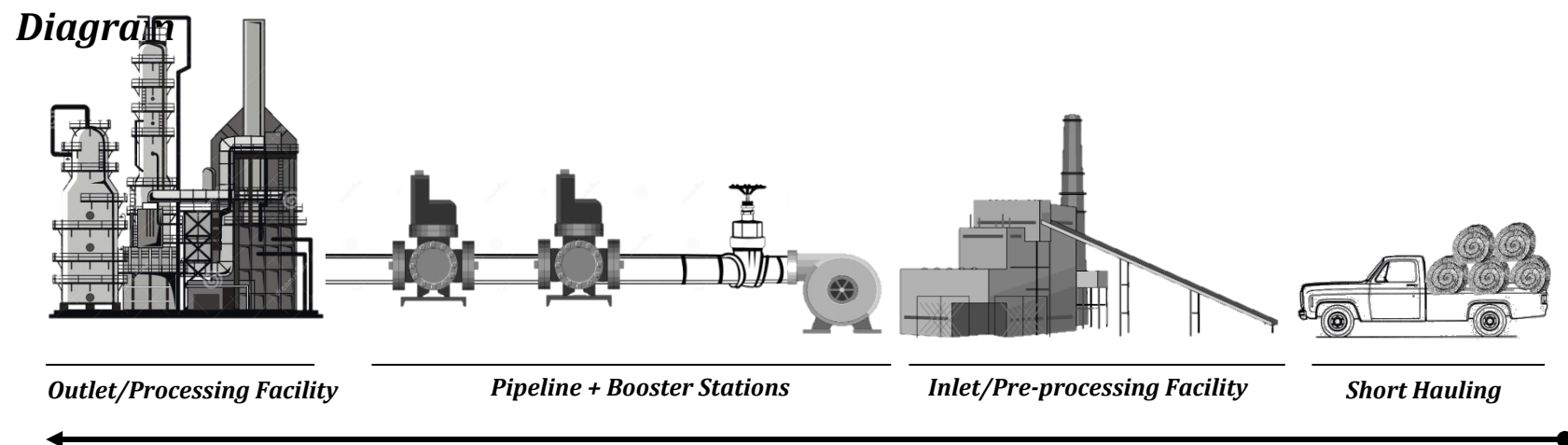
Wheat Straw





ECONOMIC FEASIBILITY

Agricultural and Forest Residue Biomass Pipeline Hydro-transport Process Flow



Research Objective

- ❑ *Study the economic feasibility of pipeline hydro-transport of agricultural and forest residue biomass*
 - ❑ *Cost of transportation*
 - ❑ *Capacity and distance*



TECHNO-ECONOMIC MODELING

General Technical Parameters

Item		Description/Value
Pipeline capacity		250,000 to 4,000,000 M dry t/yr
Average transportation distance		50 to 300 km
Biomass particle type		wheat straw and woodchips
Biomass particle size	Agricultural	Nominal: <3.2, 3.2, 6.4, 19.2 mm (d_{50} : 1.9 to 8.29 mm)
	Forest	d_{50} : 1.9 to 7.18 mm
Particle saturated moisture content	Agricultural	82%
	Forest	70%
Saturated biomass particle density	Agricultural	1050 kg/m ³
	Forest	1115 kg/m ³
Dry matter solid mass content	Agricultural	2 to 8.8%
	Forest	2 to 7.2%
Slurry velocity		1.5 to 4.5 m/s
Velocity of water in water return pipeline		2 m/s
Slurry pressure drop correlation		$\Delta H/L = [\sum_{n=1}^3 (\alpha_n S^n + \beta_n V^n + \gamma_n C^n d^n + \delta_n V^n C^n d^n)] (D/D_0)^{-1.2}$ $\left(\frac{i_m - i}{i} \right) = 2.51 C_v \left(\frac{4 g D_{pipe}}{V_m^2} \right)^{1.42}$
Slurry and water pump efficiency		80%
Maximum pressure of the pump		3100 kPa



TECHNO-ECONOMIC MODELING (CONT'D)

General Economic Parameters

Item	Values
Inflation rate	2.1%
Discount rate	10%
Life of pipeline	30 yr
Life of pump	20 yr
Capacity factor of pipeline	0.85
Maintenance cost of	
- equipment	3% of capital cost
- pipeline	0.5% of capital cost
Power cost	50 \$/MWh
Engineering cost	10% of total capital cost
Contingency cost	5% of total cost
Scale factor	0.75

Cost of biomass transportation by truck in North America (2014 USD)

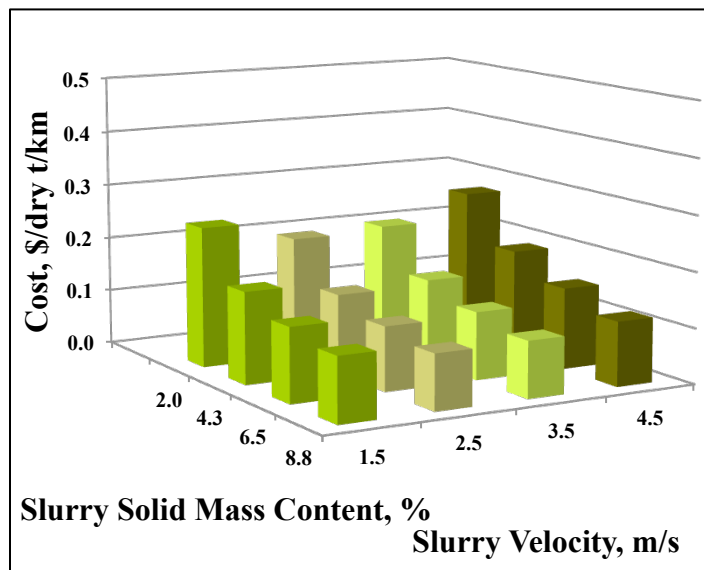
Biomass	DFC (\$/dry t)	DVC (\$/dry t/km)	Total Cost (150 km - \$/dry t)
Wheat straw	6.66	0.27	47.16
Corn stover (NREL)	9.45	0.24	45.45
Switchgrass	10.77	0.15	33.27
Hay and forage	9.20	0.16	33.2
Hay (less than 100 km)	9.02	0.40	69.02



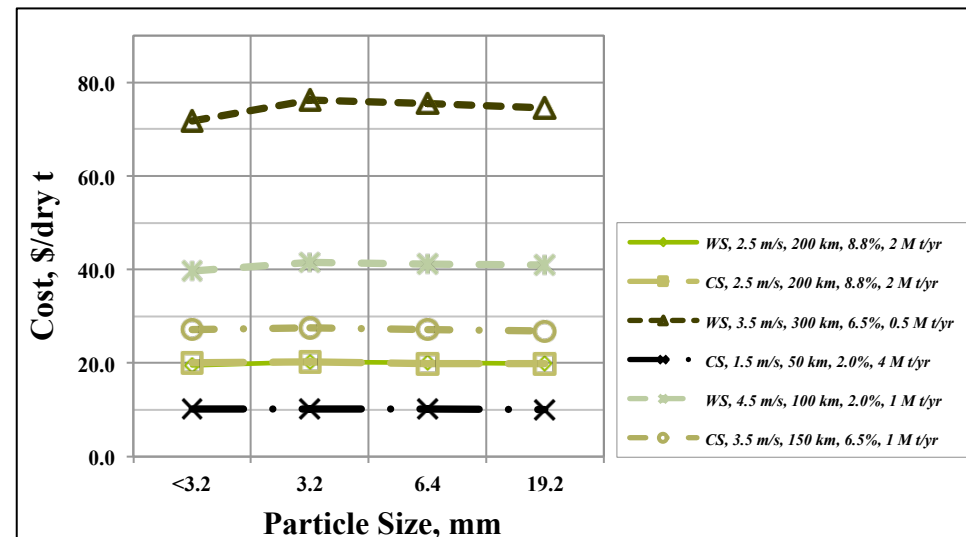
SENSITIVITY ANALYSIS

Effective Variables:

(1) biomass particle type, (2) biomass particle size, (3) pipeline capacity, (4) pipeline length, (5) slurry solid mass content, (6) slurry velocity



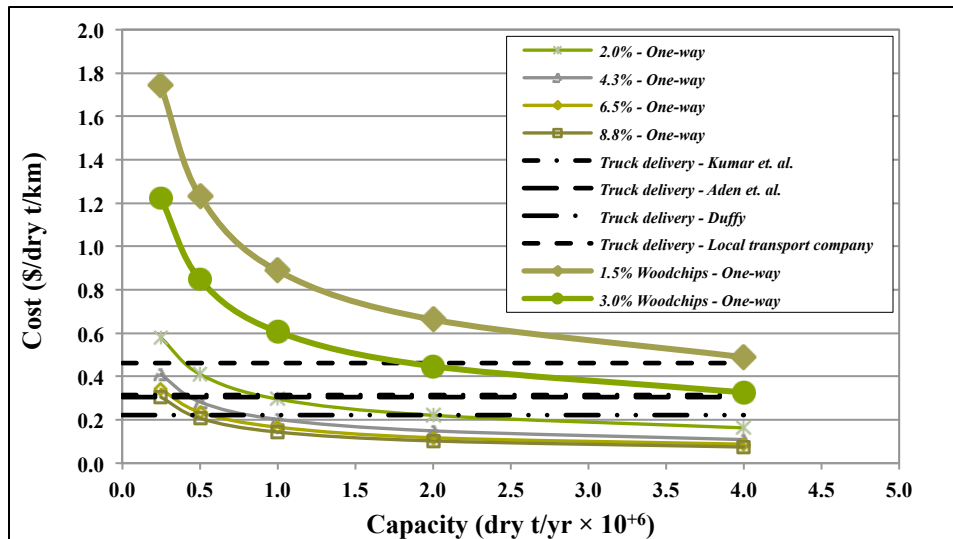
Distance variable cost of one-way pipeline hydro-transport of 2,000,000 dry t/yr of <3.2 mm wheat straw particles over a 200 km distance as a function of slurry velocity and solid mass content



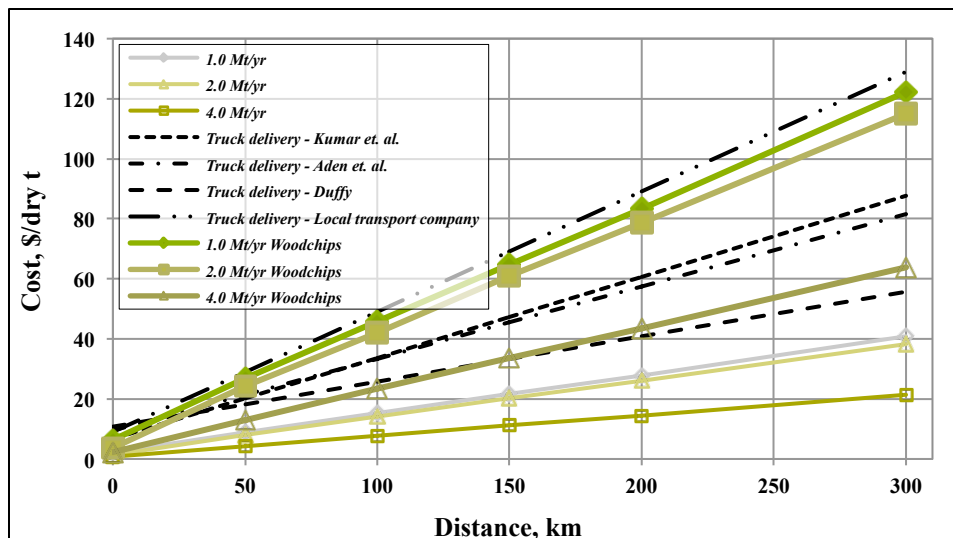
Cost of pipeline transport of various biomass particle sizes



RESULTS (one-way pipeline)



Costs of pipeline hydro-transport of <3.2 mm wheat straw particles , as well as woodchips at 2.5 m/s over 150 km as a function of pipeline capacity and slurry solid mass content



Cost of pipeline transport of 8.8% solid mass content slurry of <3.2 mm wheat straw particles and 3.0% solid mass content of woodchips at 2.5 m/s as a function of pipeline length and capacity



CONCLUSIONS

- ☐ *Agricultural residue biomass can be successfully pipelined over a wide range of particle sizes and slurry concentrations*
- ☐ *Wood fibres behave similar to wheat straw fibres when pumped into pipeline*
- ☐ *Pipeline transport of wood chips is limited by the particle size and slurry concentration*
- ☐ *Wood chips behave similar to conventional solids when pumped into pipeline*
- ☐ *Numerical correlations previously developed for fibrous agricultural residue biomass could be well used to predict the friction loss behavior of wood fibres*
- ☐ *The performance of the pump handling fibrous forest and agricultural residue biomass is positively affected vs. the pump handling water only*
- ☐ *Savings in pumping power could be obtained by replacing large chips by fine fibrous chips*



CONCLUSIONS

- ❑ *Numerical correlations developed for fibrous agricultural residue biomass could be well used to predict the friction loss behavior of wood fibres*
- ❑ *There is no concern with regard to the critical settling velocity of fibrous biomass particles in pipelines*
- ❑ *Economically considering, pipeline hydro-transport of agricultural residue biomass is favorable compare to truck mode of delivery*
- ❑ *Understanding the mechanical behavior of agricultural residue and wood chips biomass helps to optimize the design and the operating conditions of biomass pipelines and enable bio-based energy facilities to achieve higher capacities*



APPLICATIONS

- ☐ *Large-scale transport of biomass feedstock (agricultural and forest residue) for*
 - ☐ *Bio-fuel production via*
 - ☐ *Fermentation (bio-ethanol production)*
 - ☐ *Hydrothermal liquifaction*
 - ☐ *Hydrothermal gasification*
 - ☐ *Plantrose process (uses supercritical water to reduce costs in conversion of biomass to cellulosic sugars)*
 - ☐ *Pulp and paper production*



ACKNOWLEDGEMENT

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THANKS

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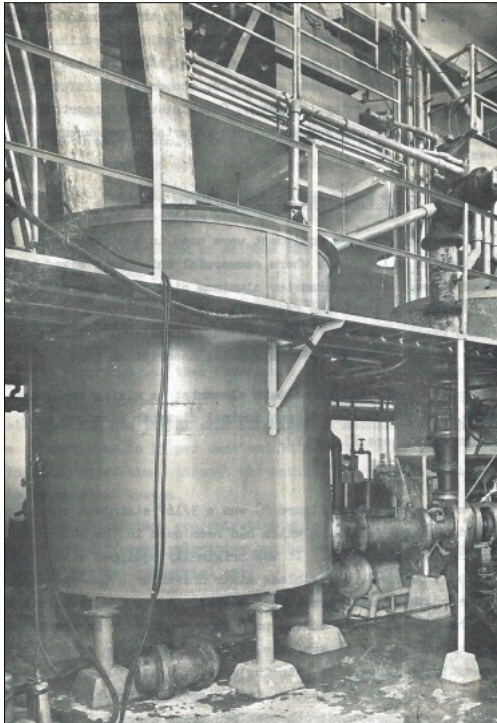
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HISTORY OF FOREST RESIDUE BIOMASS PIPELINE HYDRO-TRANSPORT



Part of the PAPRICAN pilot plant

Photo credit: Pulp and Paper Research Institute of Canada, 1960

- ❑ In **1958**, *Elliott and de Montmorency* at *Pulp and Paper Research Institute of Canada* installed a pilot plant comprised of 160 m of 200 mm diameter aluminum pipe to study the hydraulic transport of Spruce and Balsam fir wood chips in pipelines [1].
- ❑ In **1962**, the R&D section of the *Shell Pipeline Company* studied hydro-transport of wood chip-water mixtures on a closed-circuit commercial pipeline facility of 1220 m length and 200 mm diameter at Houston, Texas [2].
- ❑ In **1963**, *Faddick* presented measured the friction loss in wood chip pipelines based on studies with a 100 mm diameter aluminum pipe at *Queen's University in Kingston, Ontario* [3].

[1] Elliott DR, de Montmorency, WH; Pulp and Paper Institute of Canada; 1963.

[2] O'donnell JP; Oil and Gas Journal; 1964.

[3] Faddick RR; Kingston, Ontario: Queen's University; 1963.